

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for the coammoximation of at least two ketones which comprises reacting a mixture of at least one cyclic ketone and at least one further ketone with ammonia, hydrogen peroxide, a catalyst which essentially consists of silicon, titanium and oxygen, ~~in the presence of a solvent~~ in one step to give a corresponding mixture of ketone oximes.

Claim 2 (Previously Presented): The process as claimed in claim 1, wherein, in addition, at least one ammonium salt is used as a cocatalyst.

Claim 3 (Previously Presented): The process as claimed in claim 1, wherein a mixture of two or more cyclic ketones selected from the group consisting of cyclic ketones having 5 to 20 carbon atoms is utilized.

Claim 4 (Previously Presented): The process as claimed in claim 3, wherein a mixture of two or more cyclic ketones selected from the group consisting of cyclic ketones having 6 to 12 carbon atoms is utilized.

Claim 5 (Previously Presented): The process as claimed in claim 4, wherein, as mixture of cyclic ketones, a mixture of cyclohexanone and cyclododecanone is utilized.

Claim 6 (Previously Presented): The process as claimed in claim 1, wherein ammonia at a concentration of at least 20% in water, or pure ammonia is utilized.

Claim 7 (Previously Presented): The process as claimed in claim 1, wherein aqueous hydrogen peroxide is used at a concentration of 10-70%.

Claim 8 (Previously Presented): The process as claimed in claim 1, wherein the catalyst used is titanium silicalite.

Claim 9 (Previously Presented): The process as claimed in claim 1, wherein, as a cocatalyst, an ammonium salt of a mineral acid and/or of a carboxylic acid is utilized.

Claim 10 (Previously Presented): The process as claimed in claim 2, wherein the cocatalyst is generated in the reaction mixture in situ from a Brönsted acid and ammonia.

Claim 11 (Previously Presented): The process as claimed in claim 2, wherein the at least one ammonium salt is present in the reaction mixture at a concentration of 0.001 to 1 mol/kg.

Claim 12 (Previously Presented): The process as claimed in claim 1, wherein an at least partially water-miscible solvent, or a water-immiscible solvent is utilized as the solvent.

Claim 13 (Previously Presented): The process as claimed in claim 12, wherein, a water-immiscible solvent is utilized in combination with an interphase contactor.

Claim 14 (Previously Presented): The process as claimed in claim 13, wherein, the interphase contactor comprises alkanesulfonates and/or quaternary ammonium salts utilized at a concentration of 0.01 to 5% by weight, based on the total reaction mixture.

Claim 15 (Previously Presented): The process as claimed in claim 1, wherein the reaction temperature is in the range from 20 to 150°C.

Claim 16 (Previously Presented): The process as claimed in claim 15, wherein the reaction temperature is in the range from 50 to 120°C.

Claim 17 (Previously Presented): The process as claimed in claim 1, wherein the coammoximation is carried out in a continuous or in a batchwise reaction system.

Claim 18 (Previously Presented): The process as claimed in claim 1, wherein the reaction is carried out at a pressure of 1 to 10 bar.

Claim 19 (Previously Presented): A method for preparing lactams by Beckmann rearrangement comprising utilizing the mixture of ketone oximes prepared by the process as claimed in claim 1.

Claim 20 (Previously Presented): The method as claimed in claim 19, wherein the lactams prepared are at least one selected from the group consisting of caprolactam, enantholactam, caprylolactam, pelargonolactam, decanolactam, undecanolactam and lauro lactam.

Claim 21 (New): The process as claimed in claim 1, wherein the coammoximation is performed in the presence of a solvent in the one step to give a corresponding mixture of ketone oximes.